

## Calorimetric and PVT Measurements of {n-Hexane+1-Hexanol} up to 473 K and 20 MPa

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The binary {n-hexane + 1-hexanol} may be considered as a model system to study association phenomena in a binary mixture of two homomorph components having the same number of carbon atoms. The system has been studied at atmospheric pressure in a narrow temperature range by Roux et al [1]. The experimental data has been extended to high pressures and high temperatures by Grolier et al [2-3] by measurements of isobaric thermal expansivities from 303 K to 503 K and pressures up to 400 MPa. From these data, excess enthalpies, heat capacities and specific volumes have been estimated, using the saturation curve data as a reference. In this work, the excess enthalpies  $H^E$  and heat capacities  $c_p$  have been determined from direct experimental measurements over the temperature range 323 K to 473 K and in the pressure range from 5 MPa to 20 MPa. The measurements have been carried out using differential heat flux calorimetric techniques developed in our laboratory [4-5]. The excess volumes  $V^E$  were measured at temperatures from 303 K to 423 K and pressures from 5 to 20 MPa. The aim of the present work is to compare the  $H^E$ ,  $c_p$  and  $V^E$  data estimated from expansivities with the data obtained by direct experimental measurements. Results obtained previously combined with experimental results provide a wealth of calorimetric and PVT data over extended ranges of temperature and pressures for the model system considered. Finally, our experimental excess enthalpies  $H^E$  have been compared with the predicted values obtained using the DISQUAC model.

### REFERENCES

- [1] Roux A.H., Roux-Desgranges G., Grolier J-P.E.: Fluid Phase Equilibria, 89, 57-88 (1993)
- [2] Grolier J-P.E., Randzio S.L.: Fluid Phase Equilibria 133, 35-44 (1997)
- [3] Randzio S.L., Grolier J.P.E., Quint J.R.: Fluid Phase Equilibria 110, 341-359 (1995)
- [4] Mathonat C., Hynek V., Majer V., J-P. Grolier : J. Sol. Chem., 23, 1161-1182 (1994)
- [5] Coxam J-Y., Quint J.R., Grolier J-P.E.: J. Chem. Thermodyn., 23, 1075-1083 (1991)